DAFTAR SIMBOL

Simbol	Keterangan	Satuan
W	*Circulating Water Pump*	(kg/s)
P	Laju Aliran Masuk ke Kondensor	(kg/s)
Q	*Flow Condensate Water*	(kg/s)
S	Laju Aliran SJAE	(kg/s)
C	*Extraction LP Heater 3*	(kg/s)
B	*Extraction LP Heater 2*	(kg/s)
A	*Extraction LP Heater 1*	(kg/s)
M	Laju Aliran *Make Up Water*	(kg/s)
R	Laju Aliran dari *Fuel Oil Heater*	(kg/s)
Q_{AVG}	Rata-rata *Flow Condensate Water*	(kg/s)
K	Aliran Uap Masuk *Air Ejector*	(kg/s)
W_f	Aliran Bahan Bakar	(kg/s)
h_p	*Enthalpy Steam Out LP Turbin to Condensor*	(kJ/kg)
h_s	*Enthalpy Drain Air ejecor*	(kJ/kg)
h_{21}	*Enthalpy Drain Heater to Condensor*	(kJ/kg)
h_M	*Enthalpy Make Up Water*	(kJ/kg)
h_R	*Enthalpy Steam to FO Heater*	(kJ/kg)
h_Q	*Enthalpy FW Out Kondensor to Ejector*	(kJ/kg)
h_{Wout}	*Enthalpy Circulating Water Out Condensor*	(kJ/kg)

h_{Winlet}	*Enthalpy Circulating Water Inlet Condensor*	(kJ/kg)
h_{oi}	*Enthalpy Steam to FO Heater*	(kJ/kg)
h_{oa}/h_g	*Enthalpy FO Heater Cell*	(kJ/kg)
h_{10}	*Enthalpy Feed Water out LP HTR 3 to Deaerator*	(kJ/kg)
h_{13}	*Enthalpy Extraction Steam to LP HTR 3*	(kJ/kg)
h_{14}	*Enthalpy Feed Water Out LP HTR 2 to LP HTR 3*	(kJ/kg)
h_{15}	*Enthalpy Drain LP Heater 3*	(kJ/kg)
h_{16}	*Enthalpy Extraction Steam to LP Heater 2*	(kJ/kg)
h_{17}	*Enthalpy Feed Water Out LP HTR 1 to LP HTR*	(kJ/kg)
h_{18}	*Enthalpy Drain LP Heater 2*	(kJ/kg)
h_{19}	*Enthalpy Extraction Steam to LP Heater 1*	(kJ/kg)
h_{20}	*Enthalpy Feed Water out Air Ejector to LP HTR*	(kJ/kg)
Q_k	*Condensor Heat Load*	(W)
C_p	*Spesifik Heat*	(J/kg^{0}C)
ΔT	*Temperature Rise*	(^{0}C)
FO	Beban pemanas bahan bakar	(W)
A_0	*Cooling Surface Area*	(m^2)
OD	*Outside Diameter*	(m)
L	*Effective Tube Length*	(m)
N_t	*Total Number Tube*	
ΔTm	*Logaritma Mean Temperature Different*	(^{0}C)

ΔTi	*Different Between Saturation Steam Temperature and inlet Circulating Water Temperature*(^{0}C)	
ΔTo	*Different Between Saturation Steam Temperature and outlet Circulating Water Temperature*(^{0}C)	
V	*Circulating Water Velocity*	(m/s)
A_t	*Luas Aliran Air Pendingin*	(m^2)
ρ	*Density*	(kg/m^3)
ρv	*Vapor Density*	(kg/m^3)
ID	*Inside Diameter*	(m)
U_0	*Overall Coefficient Heat Transfer*	$(\frac{W}{m^2\ ^0C})$
C_1	*Dimensional Factor Depending upon Tube outr Diameter*	$(\frac{W}{m^2\ ^0C})$
C_2	*Dimensional Corectin factor for circulating water inlet temperatur*	(^{0}C)
C_3	*Dimensional Corectin factor for tube material and gauge*	
C_4	*Dimensional Cleannis Factor*	
h_{fi}	*Inside Dirt Coefficient coefficient*	$(\frac{W}{m^2\ ^0C})$
h_o	*Outside fluid film coefficient*	$(\frac{W}{m^2\ ^0C})$
h_i	*Inside fluid film coefficient*	$(\frac{W}{m^2\ ^0C})$
h_{fo}	*Outside Dirt Coefficient coefficient*	$(\frac{W}{m^2\ ^0C})$
k	*Thermal Conductivity of the tube wall material*	$(\frac{W}{m^2\ ^0C})$
g	*Gravitation Accelearation*	(m/s^2)

μ	*Condensate Viscosity*	(Ns/m^2)
W_c	*Total condensate flow*	(kg/s)
N_r	*Average number of tube in a vertical row*	
Re	*Reynold Number*	
Pr	*Prandt Number*	
Nu	*Nusselt Number*	
ΔP	*Pressure Drop*	(Pa)
H	*Total Head*	(m)